

FORM-PTO-1390 U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE ATTORNEY'S DOCKET NUMBER (Rev. 12-29-99

INTERNATIONAL FILING DATE

TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371

022701-915

U.S. APPLICATION NO. (If k 9/₂72 PRIORITY DATE CLAIMED

ation:

DEC 2 6 2000

PCT/FR99/01524 TITLE OF INVENTION

: 17

6.

0

18.

INTERNATIONAL APPLICATION NO

24 June 1999

25 June 1998

METHOD FOR EVAPORATING AMINONITRILE APPLICANT(\$) FOR DO/EO/US

Gérald BOCQUENET, Henri CHIARELLI and Philippe LECONTE

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other This is a FIRST submission of items concerning a filing under 35 U.S.C. 371.

This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371.

This is an express request to begin national examination procedures (35 U.S.C. 371(f)) at any time rather than until the expiration of the applicable time limit set in 35 U.S.C. 371(b) and the PCT Articles 22 and 39(1).

X A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.

A copy of the International Application as filed (35 U.S.C. 371(c)(2))

is transmitted herewith (required only if not transmitted by the International Bureau).

has been transmitted by the International Bureau

is not required, as the application was filed in the United States Receiving Office (RO/US)

A translation of the International Application into English (35 U.S.C. 371(c)(2)).

0 10 Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))

are transmitted herewith (required only if not transmitted by the International Bureau).

have been transmitted by the International Bureau.

have not been made; however, the time limit for making such amendments has NOT expired.

have not been made and will not be made.

A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).

An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).

A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).

items 11. to 16. below concern other document(s) or information included:

An Information Disclosure Statement under 37 CFR 1.97 and 1.98.

An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included

A FIRST preliminary amendment.

A SECOND or SUBSEQUENT preliminary amendment.

14 A substitute specification.

15. A change of power of attorney and/or address letter.

Other items or information:

1) International Preliminary Examination Report

2) International Search Report

U.S. APPLICATION NO. (If known 1 see 37.0 F.B. 140) 5 9 8 INTERNATIONAL APPLICATION NO PCT/FR/99/01524					ATTOR 022		NEY'S DOCKET NUMBE
17. 🛛	The following	fees are submitted:			CAL	CULATIONS	PTO USE ONLY
Basic Nati	onal Fee (37 C	CFR 1.492(a)(1)-(5)):					
Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO							
Interr	national prelim	inary examination fee (37 CF		\$860.00 (970)			
Interr but in	national prelim nternational se	inary examination fee (37 CF arch fee (37 CFR 1.445(a)(2	R 1.482) not paid to USPTO)) paid to USPTO	\$710.00 (958)			
Interr but a	national prelim Il claims did n	inary examination fee paid to ot satisfy provisions of PCT A	USPTO (37 CFR 1.482) Article 33(1)-(4)	\$690.00 (956)			
Internand a	national prelim Ill claims satis	inary examination fee paid to fied provisions of PCT Article	USPTO (37 CFR 1.482) 33(1)-(4)	\$100.00 (962)			
		ENTER	APPROPRIATE BASIC F	EE AMOUNT =	\$	860.00	
Surcharge months fro	of \$130.00 (om the earliest	154) for furnishing the oath of claimed priority date (37 CF	or declaration later than R 1.492(e)).	20 🗆 30 🗆	\$	0.00	
	aims	Number Filed	Number Extra	Rate			
Total Clain	ns	13 -20 =	0	X\$18.00 (966)	\$	0.00	
Independe	nt Claims	1 -3 =	0	X\$80.00 (964)	\$	0.00	
Multiple de	pendent claim	n(s) (if applicable)		+ \$270.00 (968)	\$	0.00	
Part I			TOTAL OF ABOVE CA	LCULATIONS =	\$	860.00	
Reduction filed (Not	for 1/2 for fili e 37 CFR 1.9	ng by small entity, if applicab , 1.27, 1.28).	le. Verified Small Entity state	ment must also be	\$	0.00	-
vii.				SUBTOTAL =	\$	860.00	
Problemsing fee of \$130.00 (156) for furnishing the English translation later than 20 30 months from the earliest claimed priority date (37 CFR 1.492(II)).					s	0.00	
14 mg/			TOTAL N	ATIONAL FEE =	\$	860.00	
an appropr	ording the end	closed assignment (37 CFR 1 et (37 CFR 3.28, 3.31). \$4	.21(h)). The assignment must 0.00 (581) per property +	be accompanied by	\$	0 00	
			TOTAL FEE	S ENCLOSED =	\$	860.00	
Sept.						mount to be:	
						refunded	\$
					_	charged	\$
a. 🗆 b. 🏻	to solve the above locally cholosed.						Process Aut
c. 🛛	sheet is enclosed.						
	ACCOUNT NO.	02-4800. A duplicate copy	of this sheet is enclosed.				
NOT! must	NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.						
SEND ALL	CORRESPON	DENCE TO:		r			
		Stepno, Esquire	LLP SIGN	ather L Sd			
	P.O. Box 1			thew L. Schneider			
	(703) 836-		NAM			-	
	Date: Dec	ember 26, 2000	32,8 REGIS	STRATION NUMBER			

09/720598 526 Rec'd PCT/PT0 26 DEC 2000

Patent Attorney's Docket No. <u>022701-915</u>

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Patent Application of)
Gérald BOCQUENET et al.) Group Art Unit: Unassigned
Application No.: Corresponds to International Application No. PCT/FR99/01524) Examiner: Unassigned
International Application Filed: June 24, 1999)
For: METHOD FOR EVAPORATING AMINONITRILE)))

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents Washington, D. C. 20231

Sir:

Preliminary to examination of the above-identified application, kindly amend the application in the following manner.

IN THE CLAIMS:

Kindly amend Claims 3-9 and 13 in the following manner.

Claim 3, line 1: delete "claims 1" and insert therefor -- claim 1, --; and line 2: delete "and 2.".

Claim 4, line 1: delete "claims 1 to" and insert therefor -- claim 1, --; and line 2: delete "3.".

- Claim 5, line 1: delete "claims 1 to" and insert therefor -- claim 1 --; and line 2: delete "4,".
- Claim 6, line 1: delete "claims 1 to" and insert therefor -- claim 1 --; and line 2: delete "5.".
- Claim 7, line 1: delete "claims 1 to" and insert therefor -- claim 1 --; and line 2: delete "6,".
- Claim 8, line 1: delete "claims 1 to" and insert therefor -- claim 1 --; and line 2: delete "7,".
- Claim 9, line 1: delete "claims 1 to" and insert therefor -- claim 1 --; and line 2: delete "8,".
- Claim 13, line 1: delete "claims 1 to" and insert therefor -- claim 1 --; and line 2: delete "12,".

REMARKS

By way of the foregoing amendments to the claims, Claims 3-9 and 13 have been amended to delete the multiple dependency.

Early and favorable consideration with respect to this application is respectfully requested.

Respectfully submitted,

BURNS, DOANE, SWECKER, & MATHIS, L.L.P.

Matthew L. Schneider Registration No. 32,814

P. O. Box 1404

Alexandria, Virginia 22313-1404

Phone: (703) 836-6620

Date: December 26, 2000

10

15

1 PROCESS FOR VAPORIZING AMINONITRILE

The present invention relates to the vaporization of aminonitrile and water under conditions which limit or eliminate the formation of heavy byproducts, especially aminocarboxylic acid oligomers.

The reaction between an aminonitrile and water results in the formation of lactam, especially caprolactam when 6-aminocapronitrile is employed.

This reaction can be carried out in liquid phase with heating and under elevated pressure. It can also be carried out in vapour phase. For this second embodiment, it is therefore necessary to convert the aminonitrile and the water to the vapour state. For examples of carrying out aminonitrile hydrolysis in vapour phase reference may be made, in particular, to the patent EP-A-0 659 741 and the international application WO-A-96/22974.

The choice of the manner of vaporization of the aminonitrile and water is not trivial.

20 In fact, it is possible to consider forming a liquid water/aminonitrile mixture and then heating this mixture to a temperature sufficient to vaporize the two components. In this case, the formation of heavy compounds having an amide function or carboxylic salt function (oligomers) is observed. These compounds are 25 capable of attaching themselves, at least in part, to the catalyst and so reducing its service life.

10

15

Furthermore, they deposit in the apparatus, and foul it. This necessitates periodic cleaning of the said apparatus and hence the relatively frequent shutdown of the plant, with all the economic consequences, as can be imagined.

Another technique which could be considered would be to vaporize the streams of aminonitrile and water separately. The Applicant has noted that, at the temperatures required to vaporize the aminonitrile, it undergoes decomposition, in considerable proportions, to give a compound of the amidine or polyamidine type (condensation of two or more molecules of aminonitrile with elimination of ammonia).

In order to avoid these various drawbacks, a process for vaporizing aminonitrile and water has now been found which is characterized in that the water, in the vapour state, is used as the carrier gas for this vaporization.

The decomposition of the aminonitrile depends

on the evaporation temperature and on the residence
time of the liquid during its evaporation. In the
process of the invention, therefore, the residence time
of the liquid is minimized by the technology of the
evaporator and the water in the vapour state reduces

the partial pressure of the aminonitrile, so lowering
its evaporation temperature.

 $\label{eq:themolar} \mbox{ The molar ratio of water to aminonitrile can}$ vary greatly in the process of the invention. It

10

15

2.0

25

depends essentially on the cyclizing hydrolysis process in which the reactants will be deployed. This molar ratio between the water and aminonitrile employed is commonly between 0.5 and 100 and preferably between 1 and 20. The upper value of this ratio is not critical for the invention, although higher ratios are of virtually no interest for the hydrolysis reaction on economic grounds.

Generally, the water vapour will be at a temperature of from 120 to 600°C and preferably from 200 to 550°C.

The aminonitrile will generally be employed at a temperature of from 20 to 300°C. Preferably, this temperature will be from 100 to 250°C.

The aminonitrile/water vapour mixture is brought rapidly in a heat exchanger to a temperature at which the vaporization of the mixture is complete.

If appropriate, this temperature can be that at which the reaction between the aminonitrile and water will be conducted. Such a reaction temperature is commonly between 200 and 450°C and preferably between 250 and 400°C

The absolute pressure at which the vaporization of the aminonitrile is conducted is generally from 0.1 to 3 bar.

The aminonitrile employed in the process of the invention is more particularly a linear or branched aliphatic aminonitrile having 3 to 12 carbon atoms. 1.0

15

20

25

By way of examples, mention may be made more particularly of the aliphatic aminonitriles originating from the hydrogenation to a primary amine function of one of the two nitrile functions of dinitriles such as adiponitrile, methylglutaronitrile, ethylsuccinonitrile, dimethylsuccinonitrile, malononitrile, succinonitrile, glutaronitrile and dodecanedinitrile

The most important aminonitrile is

6-aminocapronitrile, the cyclizing hydrolysis of which
leads to caprolactam, whose polymerization yields nylon

6.

For convenience, in the text below, reference may be made more particularly to 6-aminocapronitrile (or ACN).

The process is performed with the aid of a system without retention of liquid.

order to limit the residence time of the product in liquid phase during the evaporation are of two types:

- evaporation of the aminonitrile as a film on a heated surface:

The technologies which can be employed in

- evaporation of an at least partly liquid mist of aminonitrile in the superheated water vapour; in this case, the instances of contact between liquid and hot wall are replaced by contact between gas and liquid droplets.

In the case of evaporation as a film on a

10

15

20

25

heated surface, the heat required for the evaporation is supplied on the one hand by the appreciable heat of the vapour and of the aminonitrile and on the other hand by transfer of heat across the evaporating surface. The evaporator is of the falling-film evaporator type.

The liquid can be distributed over the tubes of the evaporator in accordance with the distribution systems generally employed in this type of technology:
- supply of the at least partly liquid aminonitrile to the tube plate, then distribution of this aminonitrile in each tube:

- distribution of the at least partly liquid aminonitrile in each tube by atomization to a mist of the aminonitrile above the tube plate; this technology has the advantage over the preceding one of reducing further the residence time in liquid phase at high temperature; the liquid can be atomized by means of a nozzle which is fed with the liquid alone or, better still, by a nozzle which is fed simultaneously with the liquid and the water vapour.

In the case of evaporation in a mist with contact between gas and water droplets, all of the heat is supplied by the appreciable heat of the two components, the aminonitrile, which is at least partly in liquid phase, and the water in vapour phase.

The temperature of the water vapour and the temperature of the at least partly liquid aminonitrile

10

15

2.0

25

are selected such that the mist obtained is at a temperature which is either equal to or greater than the dew point of the water/aminonitrile mixture which makes up the said mist. Obviously, the dew point depends on the ratio of water to aminonitrile and is easily determined for the selected ratio.

Thus, by way of example, at atmospheric pressure, the dew point is $180\,^{\circ}\text{C}$ for a water/6-amino-capronitrile (ACN) ratio of 4, $110\,^{\circ}\text{C}$ for a water/ACN molar ratio of 56, $210\,^{\circ}\text{C}$ for a water/ACN ratio of 1, and $230\,^{\circ}\text{C}$ for pure ACN.

This evaporation in a mist by contact between gas and liquid droplets can be single-stage or multistage. If the evaporation is single-stage, the temperatures of the aminonitrile and of the water vapour are such that the vaporization of the liquid can be total or partial. If the evaporation is multistage, the stream of aminonitrile, preheated to 230°C, for example, is divided into a number of portions, three or four; the first portion of this liquid is mixed with the superheated water vapour, at 300°C for example, such that all of the liquid is vaporized, the temperature of the mixture reducing simultaneously to around the dew point as a consequence of the vaporization. The mixture in the vapour state is subsequently superheated, to 300°C for example, and then mixed again with the second portion of the liquid, which vaporizes in turn; the procedure is repeated for

as many times as is necessary to obtain the total vaporization of the liquid. In this process, the mist of liquid is generated at each stage by means of atomizing nozzles, the mixture being subsequently made in a volume sufficient to ensure the total evaporation of the liquid.

The system for vaporizing the aminonitrile will preferably be selected such that the dwell time of liquid aminonitrile in the said system, comprising the preheating of the said aminonitrile, is less than or equal to one minute, preferably less than or equal to 5 seconds.

 $\label{eq:the_problem} \mbox{The examples which follow illustrate the } \\ \mbox{present invention.}$

15 EXAMPLE 1

10

20

200 g/h of 6-aminocapronitrile (ACN), preheated to 230°C, and 129 g/h of water vapour at 300° C are injected through a 1 mm nozzle.

The mist thus formed is vaporized, then superheated to 300°C with the aid of an exchanger before it supplies a hydrolysis reactor containing 162 g of alumina, the said reactor being maintained at 300°C.

Over more than 400 h of operation, no reactor

fouling nor any reduction in catalytic activity

(measured by the rate of conversion of ACN at a

constant flow rate equal to 99%) was observed.

COMPARATIVE TEST 1

329 g/h of an ACN/water mixture containing 61% by weight ACN are fed into a 200 ml evaporator heated at 300 $^{\circ}$ C.

5 The gaseous mixture emerging from the evaporator is passed to a hydrolysis reactor containing 162 g of alumina, the said reactor being maintained at 300°C.

The test is stopped after 172 h of operation.

10 During this period, the rate of conversion of ACN has passed from 99% to 95%.

Following disassembly of the apparatus, the presence of a solid (nylon 6) is noted inside the evaporator and at the entrance of the hydrolysis reactor (25% of the height of the contents of the said reactor have solidified).

10

15

CLAIMS

- Process for vaporizing aminonitrile and water, characterized in that the water in the vapour state is used as the carrier gas for the vaporization.
- 2. Process according to claim 1, characterized in that the water vapour is employed at a temperature of from 120 to 600°C and preferably from 200 to 550°C.
- 3. Process according to either of claims 1 and 2, characterized in that the aminonitrile is employed at a temperature of from 20 to 300°C and preferably from 100 to 250°C.
- 4. Process according to one of claims 1 to 3, characterized in that the mixture of aminonitrile in the water vapour that is obtained is brought rapidly in a heat exchanger to a temperature at which the vaporization of the mixture is complete.
- 5. Process according to one of claims 1 to
 4, characterized in that the mixture of aminonitrile in
 20 the water vapour that is obtained is brought to the
 temperature of reaction between the aminonitrile and
 water, preferably to a temperature of from 200 to 450°C
 and, more preferably, from 250 to 400°C.
- 6. Process according to one of claims 1 to
 25 5, characterized in that the aminonitrile is a linear
 or branched aliphatic aminonitrile having 3 to 12
 carbon atoms.

- 7. Process according to one of claims 1 to 6, characterized in that the aminonitrile originates from the hydrogenation to a primary amine function of one of the two nitrile functions of a dinitrile selected from adiponitrile, methylglutaronitrile, ethylsuccinonitrile, dimethylsuccinonitrile, malononitrile, succinonitrile, glutaronitrile and dodecanedinitrile and is preferably 6-aminocapronitrile.
- 10 8. Process according to one of claims 1 to 7, characterized in that the vaporization of the aminonitrile is conducted under an absolute pressure of from 0.1 to 3 bar
- Process according to one of claims 1 to
 8, characterized in that it is performed with a system without retention of liquid.
 - 10. Process according to claim 9, characterized in that one of the following technologies is employed:
- 20 evaporation of the aminonitrile as a film on a heated surface, in an evaporator of falling-film type;
 - evaporation of an at least partly liquid mist of aminonitrile in the superheated water vapour.
 - 11. Process according to claim 10,
- 25 characterized in that the distribution of the aminonitrile over the tubes of the falling-film evaporator is carried out by:
 - supplying the at least partly liquid

10

15

aminonitrile to the tube plate, then distributing this aminonitrile in each tube:

- distributing the at least partly liquid aminonitrile in each tube by atomization to a mist of the aminonitrile above the tube plate.
 - 12. Process according to claim 10, characterized in that the evaporation of an at least partly liquid mist of aminonitrile in superheated water vapour is single-stage or multistage.
 - 13. Process according to one of claims 1 to 12, characterized in that the system for vaporizing the aminonitrile is selected such that the dwell time of liquid aminonitrile in the said system is less than or equal to one minute, preferably less than or equal to 5 seconds.

PROCESS FOR VAPORIZING AMINONITRILE

The present invention relates to the vaporization of aminonitrile and water under conditions which limit or eliminate the formation of heavy byproducts, especially aminocarboxylic acid oligomers.

In order to avoid this drawback, a process for vaporizing aminonitrile and water has now been found which is characterized in that the water, in the vapour state, is used as the carrier gas for the vaporization.

COMBINED DECLARATION FOR PATENT APPLICATION AND POWER OF ATTORNEY (Includes Reference to Provisional and PCT International Applications)

Attorney's Docket No. 022701-915

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name;

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

METHOD F	OR EVAPORAT	ING AMINONITRILE		
- Alexandria				
tile s	pecification of wi	nich (check only one item below)	:	
	is attached here	to.		
	was filed as Un	ited States application		
	Number			
	on			
	and was amende			
	on		(if applicable).	
X	was filed as PC	Γ international application		
	Number _ PCT.	**		
	on 24 June 19			
	and was amende			
	on		(if applicable).	
I hereby state as amended b	that I have review y any amendment	wed and understand the contents referred to above.	of the above-identified specifi	cation, including the claims,
Title 37, Cod	e of Federal Regu	, , , , , , , , , , , , , , , , , , , ,		
patent or inve United States certificate or	ntor's certificate of America listed any PCT internat	benefits under Title 35, United S or of any PCT international appli below and have also identified bi ional application(s) designating at t matter having a filing date befo	cation(s) designating at least elow any foreign application(least one country other than	one country other than the s) for patent or inventor's the United States of America
PRIOR FORE	EIGN/PCT APPL	ICATION(S) AND ANY PRIOF	RITY CLAIMS UNDER 35 L	J.S.C. §119:
	UNTRY dicate "PCT")	APPLICATION NUMBER	DATE OF FILING (day, month, year)	PRIORITY CLAIMED UNDER 35 U.S.C. §119
	FR	98/08258	25 June 1998	X Yes _No
				_Yes _No
				_Yes _No
				Yes No
				Yes No
I hereby clain below.	n the benefit unde	r Title 35, United States Code §	119(e) of any United States p	
	(Application N	umber)	(Filing Date)	
	(Application N	umber)	(Filing Date)	

Page 1 of 3 (01/01)

COMBINED DECLARATION FOR PATENT	APPLICATION A	AND POWER (OF ATTORNEY (CONT	D)
(Includes Reference to Provisional and PC	T International	Applications)		

Attorney's Docket No. 022701-915

I hereby claim the benefit under Title 35, United States Code, §120 of any United States applications(s) or PCT international application(s) designating the United States of America that is/are listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in that/those prior application(s) in the manner provided by the first paragraph of Title 35, United States Code, §112, I acknowledge the duty to disclose to the Office all information known to me to be material to the patentiability as defined in Title 37, Code of Federal Regulations 5.6, which became available between the filing date of the prior application(s) and the national or PCT international filing date of this application:

PRIOR U.S. APPLICATIONS OR PCT INTERNATIONAL APPLICATIONS DESIGNATING THE U.S. FOR BENEFIT UNDER 35 U.S.C. §120:

U.S. APPLICATIONS				STATUS (check one)		
U.S. APPLICATION NUMBER		U.S. FILING DATE	PATENTED	PENDING	ABANDONED	
7.1.1						
PCT A	APPLICATIONS DESIGNATING	THE II C				
PCT APPLICATION NO.	PCT FILING DATE	U.S. APPLICATION NUMBERS ASSIGNED (if any)				
	-					

I hereby appoint the following attorneys and agent(s) to prosecute said application and to transact all business in the Patent and Trademark Office connected therewith and to file, prosecute and to transact all business in connection with international applications directed to said invention:

William L. Mathus	17,337
Robert S. Swecker	19,885
Platon N. Mandros	22,124
Benton S. Duffett, Jr.	22,030
Norman H. Stepno	22,716
Ronald L. Grudziecki	24.970
Frederick G. Michaud, Jr.	26,003
Alan E. Kopecki	25,813
Regis E. Slutter	26,999
Samuel C. Miller, III	27,360
Robert G. Mukai	28,531
George A. Hovanec, Jr.	28,223
James A. LaBarre	28,632
E. Joseph Gess	28,510
R. Danny Huntington	27,903

Eric H. Weisblatt	_30,505
James W. Peterson	26.057
Teresa Stanek Rea	30,427
Robert E. Krebs	25,885
William C. Rowland	30,888
T. Gene Dillahunty	25,423
Patrick C. Keane	32,858
B Jefferson Boggs, Jr.	32,344
William H. Benz	25,952
Peter K. Skiff	31,917
Richard J McGrath	29,195
Matthew L. Schneider	32,814
Machael G. Causes	22 506

Bruce T. Wieder
Todd R. Walters
Ronn: S Jillions
Harold R. Brown III
Allen R. Baum
Steven M. duBois
Brian P. O'Shaughnessy
Kenneth B. Leffler
Fred W. Hathaway
Wendi L. Weinstein
Mary Ann Dillahunty

33,815 34,040 31,979 36,341 36,086 35,023 32,747 36,075 32,236 24,456

21839

Address all correspondence to:

and:



21839

Gerald F. Swiss

Charles F. Wieland III

Norman H. Stepno Burns, Doane, Swecker & Mathis, L.L.P. P.O. Box 1404

Alexandria, Virginia 22313-1404

Address all telephone calls to: Norman H. Stepno

at (703) 836-6620.

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Page 2 of 3 (01/01)

FULL NAME OF SOLE OR FIRST INVENTOR	SIGNATURE	1	DATE
Gerald BOCQUENET RESIDENCE	(21) 69		03.28.01
~		CITIZENSHIP	
17, le Verger Sud, F-69360 Communay, FR POST OFFICE ADDRESS		FR	
1			
17, le Verger Sud, F-69360 Communay, FR FULL NAME OF SECOND JOINT INVENTOR, IF ANY	CICNATUDE		D. COTT
Henri CHIARELLI	SIGNATURE Charle		DATE 03.28.0/.
RESIDENCE		CITIZENSHIP	05.20.2
Lotissement Vialarzeu, Rue du 30 Mai 1944, F-69360 Communav.	FR FK (FR	
POST OFFICE ADDRESS	TR	LFK	
Lotissement Vialarzeu, Rue du 30 Mai 1944, F-69360 Communay,	FD		
FULL NAME OF THIRD JOINT INVENTOR, IF ANY	SIGNATURE .		DATE
Philippe LECONTE	Leante		03 23 01
RESIDENCE		CITIZENSHIP	
43, rue Sainte-Beuve, F-69330 Meyzieu, FR		FR	
POST OFFICE ADDRESS			
43, rue Sainte-Beuve, F-69330 Meyzieu, FR			
FULL NAME OF FOURTH JOINT INVENTOR, IF ANY	SIGNATURE		DATE
į			
RESIDENCE		CITIZENSHIP	
POST OFFICE ADDRESS			
FULL NAME OF FIFTH JOINT INVENTOR, IF ANY	SIGNATURE		DATE
RESIDENCE		T	
RESIDENCE		CITIZENSHIP	
POST OFFICE ADDRESS			
FULL NAME OF SIXTH JOINT INVENTOR, IF ANY	SIGNATURE		DATE
RESIDENCE		CITIZENSHIP	L
POST OFFICE ADDRESS			
FULL NAME OF SEVENTH JOINT INVENTOR, IF ANY	SIGNATURE		DATE
RESIDENCE		CITIZENSHIP	
POST OFFICE ADDRESS			
FULL NAME OF EIGHTH JOINT INVENTOR, IF ANY	SIGNATURE		DATE
RESIDENCE		- CANADANA	
KESIDENCE		CITIZENSHIP	
POST OFFICE ADDRESS			
1001 OFFICE ADDRESS			